

# Evaluation of Enthalpy Change due to Hydrogen Desorption for Lithium Amide/Imide System by Differential Scanning Calorimetry

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## Abstract

Enthalpy change ( $\Delta H$ ) due to hydrogen desorption (H-desorption) for the lithium amide/imide system was evaluated by differential scanning calorimetry (DSC) measurement. In order to obtain the accurate and precise value of  $\Delta H$ , we have paid special attention to following two points for correcting the raw experimental data. One is to determine a cell constant of DSC equipment, which was evaluated by using the TiO<sub>2</sub>-doped MgH<sub>2</sub> compound as a reference because of its quite similar hydrogen desorption properties to that of the lithium amide/imide system. The other is to estimate the sample amount corresponding to the H-desorption reaction from weight loss in the thermogravimetric analysis (TG). By performing both the corrections, the  $\Delta H$  value due to the H-desorption reaction from LiNH<sub>2</sub>+LiH to Li<sub>2</sub>NH+H<sub>2</sub> was evaluated to be 67 kJ/mol H<sub>2</sub>.

*Keywords:* calorimetry; thermal analysis; hydrogen absorbing materials; gas-solid reactions

## **1. Introduction**

For utilizing hydrogen as one of the secondary energies, it is necessary to establish high performance hydrogen storage (H-storage) technologies [1]. Until now, three H-storage containers of liquid hydrogen, high-pressure gas hydrogen and absorbed hydrogen in H-storage materials are considered for future practical use as H-storage tanks. Among them, H-storage materials can more densely store hydrogen than high pressure gas or liquid hydrogen. Therefore, the tank system using the H-storage materials has been considered as the most suitable one for H-storage.

From viewpoint of practical application, there are three important factors to be satisfied as a useful H-storage material. The first is to store high capacity of hydrogen, the second is to possess suitable thermodynamics and the third is to have fast kinetics for H-storage reaction. On consideration of the thermodynamics for (de-)hydrogenating reaction, the enthalpy change ( $\Delta H$ ) due to (de-)hydrogenation is one of the most important factors for evaluating whether the sample has a suitable potential for H-storage material or not. In principle, the value of  $\Delta H$  for (de-)hydrogenating reaction can be experimentally estimated by van't Hoff plot of equilibrium pressures at different temperatures obtained from pressure-composition-isothermal (PCI) measurement [2] or by direct measurement of differential scanning calorimetry (DSC) [3]. Both methods have been considered to be suitable for conventional metal hydrides. However, it is quite difficult to accurately and precisely evaluate the  $\Delta H$  value for some complex H-

storage materials composed of light elements from the van't Hoff plot [4, 5], because it takes too long time to reach an equilibrium condition from the others. Nevertheless, Kojima and Kawai have carefully measured the PCI curve on the lithium amide/imide system at some different temperatures and estimated the value of  $\Delta H$  from the van't Hoff plot to be  $-66 \text{ kJ/mol H}_2$  [6]. It is to be noted that this value is much larger than  $-45 \text{ kJ/mol H}_2$  in magnitude, which was deduced in P. Chen's report [7]. On the other hand, it is in principle possible to directly observe the  $\Delta H$  by DSC for any materials, if we can completely control the experimental conditions without an oxidation during hydrogenation or dehydrogenation process.

Until now, the DSC measurements have been performed on conventional H-storage alloys [8], but the DSC measurements have not been performed for estimating  $\Delta H$  yet because of lacking for enough fundamental works to control the experimental conditions. In this work, we tried to estimate  $\Delta H$  on the lithium amide/imide system by the DSC measurement under carefully controlled experimental condition without any exposure of the sample to air at all, and have succeeded in the evaluation of the enthalpy change  $\Delta H$  for dehydrogenating reaction from the  $\text{LiH/LiNH}_2$  composite to  $\text{Li}_2\text{NH}+\text{H}_2$ .

## 2. Experimental Details

Starting samples,  $\text{MgH}_2$  (90 %, purity),  $\text{LiH}$  (95 %),  $\text{LiNH}_2$  (95 %) and  $\text{TiCl}_3$  (98 %) used in this work were commercially purchased from Sigma-Aldrich,  $\text{TiO}_2$  nano-powder (83 %) as a catalyst was purchased from Millennium Chemicals. Detailed sample preparation of the mixture of  $\text{LiH}$  and  $\text{LiNH}_2$  with 1 mol%  $\text{TiCl}_3$  was described in our previous paper [9]. All the processes of sample preparation in this work were

performed in an Ar glove-box (MDB-2BL, Miwa MFG CO. LTD) to avoid the sample pollution due to water and oxygen in air.

DSC equipment (Q10 PDSC, TA Instruments), thermogravimetry (TG) and thermal gas desorption mass spectrometry (TDMS) equipment (TG: TG8120, Rigaku; TDMS: M-QA200TS, Anelva) were installed in two different gloveboxes (DBO-1.5KP, Miwa MFG CO. LTD. and MDB-1BL, Miwa MFG CO. LTD., respectively) to avoid exposing the sample to air at all in their measurements. In both gloveboxes, gas cycling purification systems were equipped to keep the dew point lower than  $-80\text{ }^{\circ}\text{C}$  and the oxygen concentration less than 1 ppm.

In order to evaluate the genuine enthalpy change  $\Delta H$  due to hydrogen desorption (H-desorption) reaction, it is necessary to measure both the DSC and TG-TDMS profiles for the target sample, which detects an apparent endothermic heat due to H-desorption from the sample and the amount of desorbed hydrogen corresponding to the H-desorption reaction, respectively. In this work, both the DSC and TG-TDMS measurements were performed in temperature range from  $25\text{ }^{\circ}\text{C}$  to  $450\text{ }^{\circ}\text{C}$  at a heating rate of  $5\text{ }^{\circ}\text{C}/\text{min}$ , respectively, under an argon flow with  $300\text{ ml}/\text{min}$  and a helium flow with  $100\text{ ml}/\text{min}$  using aluminum pan as a sample holder. In both the measurements, we have carefully controlled experimental conditions to realize the same H-desorption properties. The peak area corresponding to  $\Delta H$  was obtained by integrating the DSC signal in the same temperature range as the TG measurement. Under the above conditions, the DSC signal per mole  $\text{H}_2$  due to H-desorption was deduced from the amount of H-desorption estimated by TG. In this work, those DSC measurements were performed for at least three times and a good reproducibility was obtained within 1 %

error. Additionally, it is quite important to confirm that the desorption gas is only hydrogen by the TDMS measurement.

Furthermore, in order to obtain the genuine value of  $\Delta H$  from the DSC measurement, it is necessary to examine the ratio of the expected DSC signal to the detected one, which is so-called “cell constant”. The process to determine the cell constant is an essential issue of the DSC measurement because in fact the DSC sensor cannot completely detect all the heat from the sample. Generally, the cell constant depends on atmospheric conditions in the sample cell, such as temperature, flowing gas speed, gas sort and so on. To determine the cell constant in our DSC measurements, we used magnesium hydride ( $\text{MgH}_2$ ) as a reference sample, because the thermodynamic data of  $\text{MgH}_2$  is well known to be  $\Delta H = 76.1 \text{ kJ/mol H}_2$  [10]. Moreover, the hydrogen desorbing properties, e.g. the peak temperature or peak width of H-desorption, can be, in principle, controlled by doping a small amount of some transition metal oxides as catalysts to the  $\text{MgH}_2$  system [10]. The catalyzed  $\text{MgH}_2$  composite with a small amount of  $\text{TiO}_2$  possessing the single H-desorption peak at  $220 \text{ }^\circ\text{C}$  was used in this work as the reference. Because this hydrogen desorption property is almost the same as that of the lithium amide/imide system. Here, the catalyzed  $\text{MgH}_2$  composite was prepared by ball-milling the mixture of  $\text{MgH}_2$  and 1 mol%  $\text{TiO}_2$  under a hydrogen pressure of 1 MPa for 20 h.

### **3. Results and Discussions**

First of all, we investigated the carrier gas properties, which give some influence on the estimation of  $\Delta H$  in the DSC measurement. Both baselines under helium and argon flow from room temperature up to  $450 \text{ }^\circ\text{C}$  are shown in Fig.1. The result indicates that

the baseline under an argon flow condition is much leveler than that under a helium flow. The difference in the behavior should originate in their thermal conductivities, where the thermal conductivity of argon is much smaller than that of helium. Therefore, argon gas was adopted as a suitable carrier gas for the DSC measurements in this work.

The next step is to determine the cell constant around 220 °C. For that, both the TG-TDMS and DSC measurements were performed for the MgH<sub>2</sub> sample catalyzed with TiO<sub>2</sub>, the result of which is shown in Fig. 2. From the TDMS profile, a sharp peak due to H-desorption is located at about 220 °C. We also confirmed that only the hydrogen gas was desorbed from the catalyzed MgH<sub>2</sub> sample within our experimental accuracy. Therefore, from these results, it was estimated that the amount of the TiO<sub>2</sub>-catalyzed MgH<sub>2</sub> corresponding to H-desorption is 89.2 mass% in all samples as listed in Table 1. As is shown in the lower part of Fig. 2, we noticed that the DSC profile was quite similar to the TDMS one. Here, we have to take into account the thermal contribution to DSC with respect to a reduction of TiO<sub>2</sub>, which should be an exothermic reaction. From our recent results of the XAFS measurement for the Ti K-edge, we confirmed that the valence state of Ti in the catalyzed MgH<sub>2</sub> did not change before and after the thermal analyses up to 350 °C [11]. Furthermore, even if TiO<sub>2</sub> was remained after the catalyzing treatment, the amount of TiO<sub>2</sub> should be much less than 1 mol%. Therefore, the thermal contribution from the reduction should be negligible. Even after considering the amount of reference sample by TG-TDMS profile analysis, the detected value of  $\Delta H$  is 58.5 kJ/mol H<sub>2</sub> as an average of three time measurements. This value is expected to be equal to 76.1 kJ/molH<sub>2</sub>, which is well known as the standard enthalpy change by H-desorption for MgH<sub>2</sub>. Therefore, the cell constant was estimated to be 1.30 around 220 °C. On the other hand, it should be noted that the cell constant in the case of no H-desorption

reaction was determined to be 1.08 around 160 °C from the melting reaction of indium metal itself. Surely, this value is smaller than that in the case of H-desorption reaction, indicating that the DSC sensor detects less completely heat loss from sample with gas desorption than without gas release.

Strictly speaking, since the DSC measurements in the above examination were performed under an inert gas flow at about 200 kPa in the absolute pressure, we should take account of the contribution of “work ( $p\Delta V$ )” by hydrogen gas evolution to atmosphere on H-desorption reaction. However, this contribution was roughly estimated to be  $100 \text{ [kPa]} \times 0.0224 \text{ [m}^3] \sim 2 \text{ [kJ/mol H}_2]$  on the standard condition, which corresponds to increase in a few % of the standard enthalpy change of 76.1 kJ/mol H<sub>2</sub>. Therefore, we ignored this small contribution in this examination, indicating that our evaluation has less than 3 % error on the accuracy.

In the same way, the evaluation of  $\Delta H$  was performed on the lithium amide/imide target system. Figure 3 shows the results of the TDMS-TG and DSC measurements for the ball-milled mixture of LiH and LiNH<sub>2</sub> catalyzed with 1 mol% TiCl<sub>3</sub>. As is evident from the upper part of Fig. 3, the TDMS profile shows that the target sample desorbs only hydrogen gas without any ammonia emission in our experimental accuracy. Therefore, the TG value was available for the determination of the amount of sample taking place of the H-desorption reaction. As is shown in Table 1, the amount of target sample corresponding to H-desorption was evaluated to be 88.1 mass% in the whole composite. From the peak area of the DSC profile in Fig. 3, the enthalpy change was detected to be 51.2 kJ/mol H<sub>2</sub> as an average. In this case, since the peak temperature of H-desorption was almost 220 °C as well as that of the reference (TiO<sub>2</sub>-catalyzed MgH<sub>2</sub>), we used the value of 1.30 as the cell constant for the evaluation of the most probable

$\Delta H$  for the H-desorption. Consequently, the genuine  $\Delta H$  for the H-desorption from  $\text{LiNH}_2 + \text{LiH}$  to  $\text{Li}_2\text{NH} + \text{H}_2$  was evaluated to be 67 kJ/molH<sub>2</sub>, where the sample amount corresponding to H-desorption and the cell constant used for evaluation of  $\Delta H$  were listed in Table 1 as well. Here, it is to be noted that the estimated value of  $\Delta H$  by the DSC measurement is in good agreement with the  $\Delta H$  value evaluated from the van't Hoff plot [6].

In the above estimation, we ignored the thermal contribution of the ammonia emission on the evaluation of the enthalpy change due to H-desorption. So far, we have really claimed that the ammonia emission should be essential for the proceeding of the H-desorption reaction in the metal-N-H system under a closed system [12]. Since the result indicated that the amount of the ammonia emission was less than 0.1 mol% of the total amount of desorbed hydrogen, the thermal contribution of the ammonia emission to the total enthalpy change was deduced to be less than 0.1%. Therefore, we conclude that the evaluated value of  $\Delta H$  is within an experimental accuracy of less than 3 % error.

#### **4. Conclusion**

In this work, we evaluated the  $\Delta H$  for H-desorption on the lithium amide/imide system by the direct measurement of DSC. For evaluating the genuine  $\Delta H$  value, we paid attention to following two points. One is carefully to determine the cell constant by using the well-known MgH<sub>2</sub> sample catalyzed with TiO<sub>2</sub>, which has quite similar H-desorption properties to the target system. The other is to evaluate the sample amount corresponding to H-desorption reaction, which was estimated by the TG measurement. From both the estimations of the cell constant and the sample purity, we were able to

accurately determine the genuine enthalpy change  $\Delta H$  to be 67 kJ/mol H<sub>2</sub> for the H-desorption reaction from LiH + LiNH<sub>2</sub> to Li<sub>2</sub>NH + H<sub>2</sub>.

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**Table 1.** Purity of the sample, which is the amount of the sample corresponding to the H-desorption reaction, estimated by thermogravimetry (TG) measurement, the raw and averaged data of enthalpy change  $\Delta H$  due to H-desorption reaction for TiO<sub>2</sub>-doped MgH<sub>2</sub> sample and the ball-milled mixture of LiH+LiNH<sub>2</sub> catalyzed with a small amount of TiCl<sub>3</sub>.

	MgH <sub>2</sub> catalyzed with 1 mol% TiO <sub>2</sub>			LiH+LiNH <sub>2</sub> catalyzed with 1 mol% TiCl <sub>3</sub>		
Sample purity corresponding to H-desorption [mass.%]	89.2			88.1		
$\Delta H$ (experimental) [kJ/molH <sub>2</sub> ]	58.0	58.7	58.7	50.5	52.0	51.1
$\Delta H$ (average) [kJ/molH <sub>2</sub> ]	58.5			51.2		
$\Delta H$ (genuine) [kJ/molH <sub>2</sub> ]	76.1			66.7		

### Captions

**Figure 1.** Baselines for DSC measurements under He and Ar flowing gases with no sample

**Figure 2.** Thermal desorption mass spectrometry (TDMS), thermogravimetry (TG) and differential scanning calorimetry (DSC) profiles for TiO<sub>2</sub>-doped MgH<sub>2</sub> product as a reference sample.

**Figure 3.** Thermal desorption mass spectrometry (TDMS), thermogravimetry (TG) and differential scanning calorimetry (DSC) profiles for the ball-milled mixture of LiH and LiNH<sub>2</sub> catalyzed with 1 mol% TiCl<sub>3</sub>.

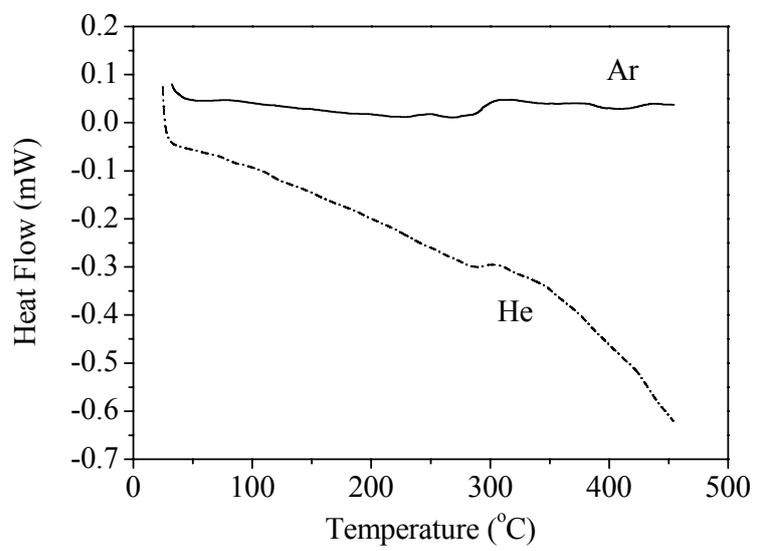


Figure 1

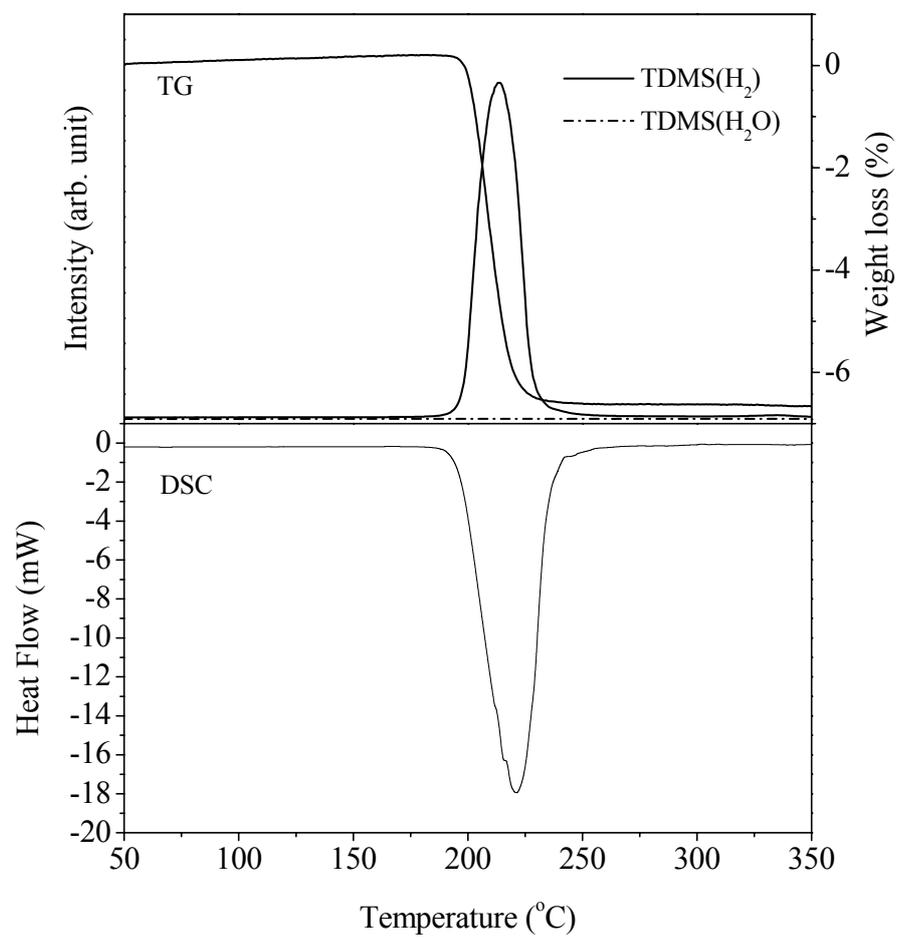


Figure 2

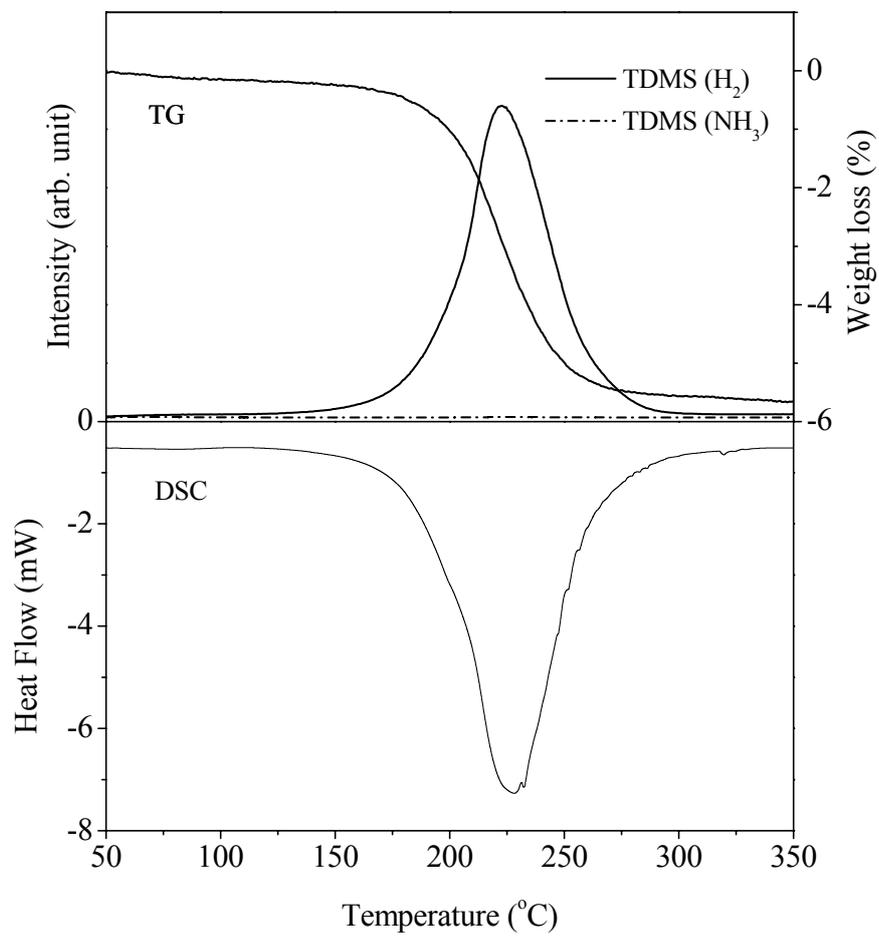


Figure 3