Synthesis and decomposition reactions of metal amides in metal-N-H hydrogen storage system

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Abstract After some metal amides $M(NH_2)$ _x such as LiNH₂, NaNH₂, Mg(NH₂)₂ and $Ca(NH₂)₂$ were synthesized by ball milling the corresponding metal hydrides MH_x under ammonia atmosphere at room temperature, their thermal decomposition properties were examined, which play important roles for designing a new family of novel Metal-N-H systems. The results indicate that the kinetics of their synthesizing reactions are faster in the order of Na amide > Li amide > Ca amide > Mg amide, while both $Mg(NH_2)$ and $Ca(NH₂)$ ₂ decompose and emit NH₃ at lower temperature than LiNH₂.

KEYWORDS Hydrogen storage, Metal hydride, Ammonia, Metal amide, Reactive ball milling.

1. Introduction

As early as 1910, Dafert and Miklauz^[1] had reported that the reaction between lithium nitride Li_3N and hydrogen H_2 had generated Li_3NH_4 , which was later proved to be a mixture of lithium amide $LiNH₂$ (1 mole) and lithium hydride LiH (2 moles) by Ruff and Goeres ^[2]. After almost one century, Chen et al.^[3] and Hu and Ruckenstein^[4] have investigated the system Li₃N as one of the hydrogen storage materials, where the hydrogenation and dehydrogenation of Li₃N were reversibly performed by the following 2step reversible reactions $^{[3]}$:

$$
Li_3N + 2H_2 \leftrightarrow Li_2NH + LiH + H_2 \leftrightarrow LiNH_2 + 2LiH \qquad (1).
$$

According to the two-step reactions in eq. (1) , Li₃N can theoretically store 10.4 wt.% hydrogen. However, the standard enthalpy change ($\sim 148 \text{kJ/mol H}_2^{\{5\}}$) of the desorption reaction at the first step was so high that a very high temperature over 430 $^{\circ}C^{[4]}$ was required for the complete recovery of Li₃N from the hydrogenated state. On the other hand, since the second step reaction has much lower standard enthalpy change (44.5kJ/mol H_2) of desorption and has still large amount of hydrogen capacity (6.5wt.%), it is worthy to be studied as one of the rechargeable hydrogen storage system, which is expressed as follows:

$$
LiNH2 + LiH \leftrightarrow Li2NH + H2, \t(2)
$$

Ichikawa et al.^[6] reported that the mixture of $LiNH₂$ and LiH doped with 1mol.% TiCl₃ by ball milling method reversibly desorbed and absorbed a large amount of hydrogen $(\sim 5.5 \text{wt.})$ % in the temperature range from 150 to 200 °C. Furthermore, the mechanism of desorption reaction (2) was experimentally examined in detail^[5,7], and the desorption has been clarified to proceed by the following two elementary reactions:

$$
2LiNH2 \rightarrow Li2NH + NH3
$$
 (3)
LiH + NH₃ \rightarrow LiNH₂ + H₂ (4)

The reaction (3) was endothermic while the reaction (4) was exothermic and has been proved to be ultra-fast in the hydrogen desorption reaction $(2)^{7}$.

Especially, some elements in groups of I-IV in the periodic table, can form their nitride, hydride and amide/imides. Among them, it still is possible to design plenty of metal-N-H systems with similar reactions to eqs. (1) and (2), which will be expected to be candidates for hydrogen storage. Quite recently, some new metal-N-H systems for hydrogen storage have been developed, such as the system composed of magnesium amide $Mg(NH_2)$ and $LiH^{[8-11]}$, the system composed of Mg(NH₂)₂ and MgH₂^[11,12], the system of Li-Ca-N-H^[9] and so on. The hydrogen storage properties of those systems are quite different among them. For instance, the system composed of $Mg(NH_2)$ and LiH has much higher equilibrium pressure for hydrogen desorption than the system of LiNH₂ and LiH^[9]. In order to understand the differences among them and to further develop the metal-N-H system as a new family of H-storage materials, the investigations on the reactions between metal hydrides MH_x and $NH₃$ and on the decomposition behaviors of the metal amides are very important and indispensable.

In this work, we investigated the novel reaction between MH_x and NH_3 at room temperature by mechanical ball milling. As a result of ball milling, their metal amides could be effectively produced in high purity. Then, we examined the thermal decomposition behaviors of these metal amides.

2. Experimental

The starting materials were purchased from Sigma-Aldrich: LiH and NaH with 95% purity, and MgH2 with 90% purity (most of the impurities is no-hydrogenated Mg), and CaH2 with 99.99% purity. All the material handlings (including weighing and loading) were performed in a glove-box filled with purified argon to keep a low water vapor concentration and a low oxygen concentration (less than 2 ppm for both) during operation using a gas recycling purification system (MP-P60W, Miwa MFG Co., LTD.). 100 mg samples and 20 steel balls of 7mm in diameter were put into a milling vessel made of hardened Cr-steel, in which 0.4 MPa NH_3 gas was filled. The ball milling was performed using a rocking mill (RM-10, SEIWA GIKEN Co., Ltd.) with a frequency of 10 Hz. To avoid an increase in temperature during milling, the milling process was interrupted every 15 min. The fraction of H_2 in the milling vessel was monitored by gas chromatographic analysis (GCA) (Shimadzu, GC8AIT). The milling vessel was refilled with 0.4 MPa NH_3 at every time after degassing until the reaction of metal hydrides with gaseous NH_3 was complete.

The quality of the products after milling was checked by X-ray diffraction (XRD) with CuK α radiation (Rigaku, RINT-2500) and elementary analysis due to oxygen combustion (Perkin Elmer 2400α CHN).

The thermal decomposition behaviors of the products were examined by thermal desorption mass spectroscopy (TDMS) (Anelva M-QA200TS) combined with thermogravimetry (TG) in the heating process up to 500 \degree C at a heating rate of 5 \degree C/min under a helium flow. This equipment has been specially set inside the glove-box filled with purified argon, which permitted simultaneous measurements of TG and TDMS without exposing the samples to any air.

3. Results and discussion

3.1 Reaction between metal hydride and NH3 by ball milling

Motivated by the reaction (4) between LiH and $NH₃$, we expected that the reactions between the alkali and alkaline earth metal hydrides and gaseous NH_3 would proceed by ball milling at room temperature according to the following reaction:

$$
MH_x + xNH_3 \to M(NH_2)_x + xH_2 \tag{5},
$$

where M represents alkali or alkaline earth metals like M=Li, Na, Mg or Ca. Figure 1 shows the kinetic properties of the reactions between MH_x and $NH₃$. The time for the completion of the reaction (5) is estimated to be 1, 2, 8 and 13 h for NaH, LiH, CaH₂ and

MgH₂, respectively, which is faster in the order of NaH > LiH > CaH₂ > MgH₂, being consistent with the inverse order of magnitude of those metals' electronegativities, i.e. Na < $Li = Ca < Mg$.

To confirm whether the corresponding metal amides were really synthesized in high quality, the products were examined by the XRD measurement. As shown in Figs. 2a, 2b and 2d, it is noticeable that the XRD patterns of the products are assigned to be almost single-phases of the corresponding metal amides $LiNH_2$, $NaNH_2$ and $Ca(NH_2)$, respectively. On the other hand, the X-ray pattern for the product prepared by milling $MgH₂$ under NH₃ for 13 h (Fig. 2c) shows a nano-structured or an amorphous phase because of showing no structural profile in it. Here, it is noted that the amorphous-like background around 20 degrees in all the XRD patterns is from the grease using for fixing the powder on the sample holder. Since it was difficult to confirm the formation of the $Mg(NH₂)$ ₂ molecule by XRD, the elementary analysis was employed to chemically analyze the concentrations of H and N in the products. The mass ratio of N to H was estimated to be 7.0 ± 0.2 wt.%, which was in good agreement with the theoretical value of 6.95 expected for Mg(NH₂)₂ molecule. In addition, the product after heat treatment at 300 °C for 1 h under NH₃ atmosphere was confirmed to be the single phase of crystallized Mg(NH₂)₂ which is shown in Fig. 2c. Thus, the above results suggest that the product after ballmilling is a nano-structured $Mg(NH_2)$ phase.

Generally, the light metal hydrides like LiH, NaH, $MgH₂$, and CaH₂ possess relatively high H densities among metal hydrides (12.7wt.% in LiH, 4.2wt.% in NaH, 7.7wt.% in MgH₂, and 4.8wt.% in CaH₂). However, their metal-H ionic-bonds are so strong that it requires quite high temperatures to complete their thermal decompositions (720 °C for LiH, 425 °C for NaH, 327 °C for MgH₂ and 650 °C for CaH₂)^{[13][14]}. Nevertheless, their extremely stable chemical bonds between metals and hydrogen are easily loosed and broken because of the interaction with the polar molecule of $NH₃$, and the ionic metal hydrides exothermically react with NH₃ into producing their amides and gaseous hydrogen.

 In order to examine how the milling process is vital for the present synthetic technique compared with the conventional synthesizing method of metal amides by heating the pure metals under NH_3 atmosphere $^{[15,16]}$, we carried out the following experiments. At the first step, LiH was kept under a $0.4MPa NH_3$ gas atmosphere for 3 h at room temperature under a static condition, but no $H₂$ was detected in the vessel by the GCA examination, indicating no proceeding of the reaction. At the next step, the sample was exposed to 0.4 MPa NH_3 gas for 3 h at 100 °C also under the static condition, but only about 1.5% H_2 was detected, indicating that only 1.5% of LiH reacts with NH₃ within 3 h at 100 $^{\circ}$ C. Thus, our experimental results indicated that it needs a very long time for proceeding of the reaction (6) without ball-milling treatment at room temperature. This may be due to the fact that LiNH₂ is first formed on the surface layer of LiH particles by reacting with NH_3 and then $NH₃$ should diffuse through the LiNH₂ surface layer to further progress the reaction with LiH located inside the particle, which would take a long time to complete the reaction. On the other hand, when LiH was mechanically milled under a $0.4MPa NH₃$ gas atmosphere at room temperature, ~ 50 % of LiH reacted with NH₃ even within 2 min (see Fig. 1). This indicates that the milling treatment leads to the acceleration of the reaction between the metal hydrides and gaseous NH3, because the milling process can bring continuous creation of fresh reactive surfaces between metal hydrides and NH3. Similarly, Dennis and Browne have reported that the bubbling of the ammonia through the molten sodium to increase the surface contact between the metals and gaseous NH₃, instead of merely conducting the gas over the surface of the metal, can greatly accelerate their interaction ^[15], which might bring similar effect to the milling treatment. However, this new technique brings no troubles caused by the melting of metals or metal amides^[16], it can be developed as one of the effective methods for the synthesis of metal amides.

3.2 Decomposition reaction of metal amides

Next, the thermal decomposition properties were examined for the above metal amides. Figure 3 shows TDMS and TG profiles obtained by heating up to 500 ºC under a heating rate of 5 °C /min for the products except NaNH₂. In our experiments, NaNH₂ did not decompose into its imide in the heating process up to 300°C. Since it easily reacted with the sample holders made of Au and Al metals, and melted and/or volatilized at higher temperatures, another suitable method is needed to clarify the decomposition behavior of NaNH₂ at higher temperatures.

As shown in Fig. 3a, the NH₃ desorption reaction from $LiNH₂$ prepared by ball milling for 2 h begins around 220 ºC and the TDMS profile shows clear double peaks around 320 ^oC and 400 ^oC. The weight loss due to the NH₃ desorption is \sim 37 wt.% up to 500 ^oC, which should correspond to the decomposition of $2LiNH₂$ into $Li₂NH$ and $NH₃$. The XRD profile also indicates that LiNH₂ fully transforms into Li₂NH after decomposition within 500 $^{\circ}$ C (Fig. 4a). Furthermore, we examined the decomposition of the sample at 320 °C corresponding to the first peak in Fig. 3a under helium flow for 2h. The results showed that the weight loss due to the NH₃ emission reached up to \sim 35wt.% and the XRD profile also showed the same structure as that in Fig. 4a. Therefore, both two peaks in the $NH₃$ desorption profile should correspond to the decompositions from $LiNH₂$ to $Li₂NH$ and be originated in some kinetic characters.

As is shown in Fig. 3b, the NH₃ gas is desorbed from $Mg(NH_2)_2$ at temperature above 175^oC and the desorption profile shows two peaks around 335 ^oC and 420 ^oC on the heating process up to 500 $^{\circ}$ C. However, the origin of appearing two-peak structure in the NH₃ desorption from $Mg(NH_2)$ is different from that of the LiNH₂ case. It was due to the existence of two-step chemical reactions, because that the XRD profile of the product after thermal desorption at 330 °C for 2h under helium flow was assigned to MgNH phase (Fig.

4b), while it transformed to Mg₃N₂ phase after the thermal desorption up to 500 °C (Fig. 4c). Therefore, the weight loss of \sim 30 wt.% due to the first step desorption of NH₃ up to around 400 °C mainly corresponded to the decomposition from $3Mg(NH₂)$ to $3MgNH$ and $3NH_3$, while the second step desorption of NH₃ leading the total weight loss up to ~ 40 wt.% until 500 °C, mainly corresponded to the decomposition of 3MgNH into Mg₃N₂ and $NH₃$.

The decomposition behavior from $Ca(NH₂)₂$ is shown in Fig. 3c as well. We notice that the NH₃ gas is emitted from 70 °C and the desorption curve takes two main peaks at 230 °C and 380 °C, respectively. According to the weight loss percent of 21%, the product after heating up to 500 °C should be a CaNH phase. However, the XRD profile can not be assigned to a well-known cubic CaNH phase (Fig. 4e). On the other hand, when the $Ca(NH₂)₂$ was heated up to 350 °C which corresponds to weight loss of 16.0 wt.% in Fig. 3c, the product could be assigned to the cubic CaNH phase (Fig. 4d). This suggests that an unknown phase transition took place during the decomposition of $Ca(NH₂)₂$ within 500 °C. The phase changes in Ca-N-H are reported in detail elsewhere $^{[17]}$. At present, it is still out of our understanding of the complicated decomposition behavior of $Ca(NH₂)₂$, which is similar to the complicated behavior in the reaction between Ca_3N_2 and $H_2^{[14]}$. Further investigation is needed to clarify the decomposition mechanism in the system of Ca-N-H.

Comparing the decomposition behaviors, it is noticeable that both the $Mg(NH₂)₂$ and $Ca(NH₂)₂$ are more unstable than $LiNH₂$ in the thermodynamic and kinetic point of view. Generally, the electronegativity of metal can affect the decomposition behavior of the corresponding metal amide. In fact, since the electronegativity of Mg is larger than that of Li, the ionic bond between the cation Mg^{2+} and anion $[NH_2]$ ⁻ would be weaker than that between $Li⁺$ and $[NH₂]⁻$ ions. This well explains the results of lower temperature decomposition and slower synthesis of $Mg(NH_2)_2$ compared with LiNH₂ in this work. Furthermore, it is noteworthy that $Mg(NH_2)$ decomposes into MgNH and finally into Mg₃N₂ within 500 °C, while LiNH₂ only decomposes into not Li₃N but Li₂NH in the same condition.

On the other hand, $Ca(NH₂)₂$ shows unusual decomposition behaviors from the viewpoint of electronegativity of metal. Because the electronegativity of Ca is smaller than that of Mg, the bond between the Ca^{2+} and $[NH_2]^-$ should be stronger than that between Mg^{2+} and [NH₂]⁻, which might qualitatively explain the difference of kinetic behavior of the reactions between CaH $_2$ /MgH $_2$ and NH $_3$ shown in Fig. 1. However, the decomposition behavior that the NH₃ desorption temperature from $Ca(NH₂)₂$ is much lower than that from $Mg(NH_2)$ ₂ (Fig. 3b and 3c) is not simply understood through the consideration of the electronegativity. This indicates that the other factors controlling the activation energy for the progress of decomposition should be considered for understanding the decomposition behavior for the amides.

According to the hydrogen desorption mechanism of $LiNH₂$ and LiH system where the decomposition reaction (3) of LiNH₂ is the first elementary step^[5], it is expected that if the metal amide more easily decomposes and emits ammonia, the hydrogen desorption properties will be much more improved. Therefore, the mixed $Mg(NH_2)$ and MH_x system would be recognized as one of the promising metal-N-H systems for hydrogen storage. In fact, the metal-N-H system composed of $Mg(NH_2)$ and LiH showed a quicker hydrogen desorption property at lower temperature than that of $LiNH₂$ and $LiH^[8-12]$. Similarly, according to the second elementary step reaction (4), the reaction between metal hydride and $NH₃$ will also effect the hydrogen desorption properties of the metal-N-H system. That is to say, the faster reaction between metal hydride and $NH₃$ can effectively transform into the corresponding metal amide and desorb hydrogen, leading to the better hydrogen storage properties. For example, since the reaction between LiH and NH₃ is faster than that of MgH₂ and NH₃, the hydrogen desorption kinetics in the system composed of 8LiH and $3Mg(NH_2)_2$ is much better than that in the system of $2MgH_2$ and $Mg(NH_2)_2^{[12]}$.

9

4. **Conclusions**

The reaction between MH_x and gaseous NH_3 was confirmed to quickly proceed at room temperature by ball milling, resulting in the synthesis of the corresponding metal amide $M(NH₂)_x$ (M=Na, Li, Mg or Ca), because the milling treatment brings the acceleration of the reaction by continuous creation of fresh reactive surfaces between metal hydrides and $NH₃$. The reaction kinetics becomes faster in the order of Na amide $>$ Li amide $>$ Ca amide > Mg amide, which corresponds to the inverse order of electronegativity of metals, i.e. Na \leq Li = Ca \leq Mg. On the other hand, both Mg(NH₂)₂ and Ca(NH₂)₂ more easily decompose and emit NH₃ at lower temperature than $LiNH₂$. Furthermore, $Mg(NH₂)₂$ decomposes into its nitride within 500° C, while LiNH₂ decomposes into not its nitride but imide up to 500 °C.

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Fig. 1. Kinetic curves of the reactions between metal hydrides and NH₃ analyzed by GCA method.

Fig.2 XRD patterns of the products obtained (a) by milling LiH under $0.4MPa NH_3$ for 2 h; (b) by milling NaH under 0.4MPa NH₃ for 1 h; (c) by milling MgH₂ under 0.4MPa NH₃ for 13 h (the inserted one) and then by annealing the sample at 300 $^{\circ}$ C in NH₃ for 1 h; (d) by milling CaH₂ under 0.4MPa NH₃ for 8 h. The symbols of $\#01$ -1168 and $\#03$ -0123 are the numbers of JCPDS file. The broad peak around 20 degrees is due to grease using for fixing the powder on the sample holder.

Fig.3 Thermal desorption mass spectrum (solid lines) and thermogravimetry profiles (dashed lines) of the metal amides during the heating process up to 500 \degree C at a 5 \degree C /min heating rate under a helium flow. (a) $LiNH₂$ made by milling LiH under 0.4MPa NH₃ for 2 h; (b) Mg(NH₂)₂ produced by milling MgH₂ under 0.4MPa NH₃ for 13 h; (c) Ca(NH₂)₂ synthesized by milling $CaH₂$ under NH₃ for 8 h.

Fig.4 XRD patterns of the products after thermal decomposition (a) the product of $LiNH₂$ after heating up to 500 °C under a helium flow; (b) the product of $Mg(NH_2)$ after thermal desorption under a helium flow at 330 °C for 2 h; (c) the product of Mg(NH₂)₂ after heating up to 500 °C under a helium flow; (d) the product of Ca(NH₂)₂ after heating up to 350 °C under a helium flow; (e) the product of $Ca(NH_2)_2$ after heating up to 500 °C under a helium flow. The JCPDS profiles of CaNH and Ca_3N_2 are shown in the below for comparison. The broad peak around 20 degrees is due to grease using for fixing the powder on the sample holder.

Fig. 1. Kinetic curves of the reactions between metal hydrides and NH3 analyzed by GCA method.

Fig.2 XRD patterns of the products obtained (a) by milling LiH under $0.4MPa NH₃$ for 2 h; (b) by milling NaH under $0.4MPa NH₃$ for 1 h; (c) by milling MgH₂ under $0.4MPa NH₃$ for 13 h (the inserted one) and then by annealing the sample at 300 $^{\circ}$ C in NH₃ for 1 h; (d) by milling CaH2 under 0.4MPa NH3 for 8 h. The symbols of #01-1168 and #03-0123 are the numbers of JCPDS file. The broad peak around 20 degrees is due to grease using for fixing the powder on the sample holder.

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